

### Assessing Technical and Economic Aspects of Nuclear Hydrogen Production for Near-term Deployment

Insights from the IAEA CRP I35006

# Acknowledgment



- Algeria Rafika Boudries
- Argentina
   Ana Bohe
- China
   Jian-Qiang Wang
- Greece
   Melpomeni Varvagianni
   Nicos Catsaros
- India

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- Japan
   Xing Yan
- Russian Federation
   Andrey Balanin
- Saudi Arabia Abdullah Alzahrani
- Turkey Hasan Özcan
- USA Shripad Revankar

Former IAEA Project Officers Ibrahim Khamis Rami El-Emam

Current IAEA Project Officers Alina Constantin Francesco Ganda

# **Overview of the CRP**

- Objective of the CRP:
  - ✓ to assess gained experience from R&D on nuclear hydrogen production in MSs and
  - ✓ to assess potential near-term deployment of nuclear hydrogen production

#### • Participation:

- ✓10 participating MSs
- ✓ 5 research contracts (Algeria, Argentina, Greece, Russian Federation, Turkey)

✓ 5 agreements (China, India, Japan, Saudi Arabia, USA)

#### Research Coordination Meetings

✓ 1st: 3-5 Dec 2018 (Vienna)
✓ 2nd: 19-21 Oct 2020 (virtual)
✓ 3rd: 15-17 Nov 2021 (virtual)

Examining the Technoeconomics of Nuclear Hydrogen Production and Benchmark Analysis of the IAEA HEEP Software

IAEA-TECDOC-1859

#### Outcomes of the past CRP:

(A) IAEA

Examining the Technoeconomics of Nuclear Hydrogen Production and Benchmark Analysis of the IAEA HEEP Software | IAEA

Contract/Agreement Country Organization ALGERIA Centre de Développement des C 22556: Assessing Technical and Economic Aspects of Nuclear Energies Renouvelables (CDER) Hydrogen Production for Near-term Deployment ARGENTINA C 22528: Upscaling of Experimental Facilities for Nuclear Hydrogen Comisión Nacional de Energía Atómica (CNEA) de Argentina Production Through Gasification of Argentine Solid Fuels CHINA Shanghai Institute of Applied A 22562: Evaluation of MW Grade TMSR-Nuclear Hydrogen Physics, Chinese Academy of Production Using Solid Oxide Electrolyser Technology Sciences GREECE National Center of Scientific C 23530: Identifying Adequate SMR Technology for Innovative H2 Research "Demokritos" Production, Compression and Storage INDIA BARC A 22635: Technical and Safety Studies for Integration of High Temperature Reactors with Iodine-Sulphur Process Based Hydrogen Production Plant and Upgradation of the Software HEEP for Economic Assessment of Hydrogen Production JAPAN JAEA A 22549: Evaluation of Nuclear Hydrogen Production Technologies and Prospectus for Deployment RUSSIAN National Research Center C 22560: Assessing Potential of High Temperature Reactor Facilities FEDERATION Kurchatov Institute of Russian Design for Hydrogen Production SAUDI Umm Al-Qura University A 22516 : Thermo-Economic Analysis and Optimization of a Large-医鼻周 ARABIA Scale Nuclear Hydrogen Production Utilizing High Temperature TURKEY Karabuk University C 22554: Economics and Integration of Hybrid Thermochemical (+ Cycles to Near Future Nuclear Reactors for Hydrogen Production USA A 22480: Safety and Scaling Analysis of Nuclear Hydrogen Purdue University Production Schemes with Current and Near Future Nuclear Plants

IAEA

# **Publications**



| Argentina/<br>CNEA                         | 2020 | Canavesio, C., Nassini, D., Nassini, H. E., Bohe, A. E., <b>Study on an original cobalt-chlorine thermochemical cycle for nuclear</b><br><b>hydrogen production</b> , International Journal of Hydrogen Energy, 45 (49), 26090-26103 (2020).<br><u>https://www.sciencedirect.com/science/article/pii/S0360319919331519</u>                         |
|--|------|--|
| China/ SINAP                               | 2019 | Guan, C., et al., Molten salt synthesis of Nb-doped (La, Sr) FeO3 as the oxygen electrode for reversible solid oxide cells,<br>Materials Letters, 245, 114-117 (2019). <u>https://doi.org/10.1016/j.matlet.2019.02.116</u>   |
|  | 2019 | Wang, J., Dai, Z., Xu, H., <b>Research Status and Prospect of Comprehensive Utilization of Nuclear Energy</b> , Bulletin of Chinese Academy of Sciences, 34, 4, 460-468 (2019).  |
| Turkey/<br>Karabuk<br>University           | 2019 | EI-Emam, R. S., Ozcan, H., <b>Comprehensive review on the techno-economics of sustainable large-scale clean hydrogen</b><br><b>production</b> , Journal of Cleaner Production 220, 593-609 (2019).<br><u>https://www.sciencedirect.com/science/article/abs/pii/S0959652619303361</u>   |
|  | 2020 | Funda, A., Ozcan, H., Turkey's industrial waste heat recovery potential with power and hydrogen conversion technologies: A techno-economic analysis, International Journal of Hydrogen Energy (2020).         https://www.sciencedirect.com/science/article/pii/S0360319920342610  |
|  | 2020 | El-Emam, R., Ozcan, H., Zamfirescu, C., Updates on promising thermochemical cycles for clean hydrogen production using nuclear energy, Journal of Cleaner Production 262 (2020)  |
| Saudi Arabia/<br>Umm Al-Qura<br>University | 2018 | <ul> <li>AlZahrani, A., Dincer, I., Modeling and performance optimization of a solid oxide electrolysis system for hydrogen production, Applied Energy, 225, 471-485 (2018).</li> <li>Modeling and performance optimization of a solid oxide electrolysis system for hydrogen production - ScienceDirect</li> </ul>                                |
|  | 2021 | <ul> <li>AlZahrani, A., Dincer, I., Exergoeconomic analysis of hydrogen production using a standalone high-temperature electrolyzer,<br/>International Journal of Hydrogen Energy, 46, 27, 13899-13907 (2021).</li> <li>Exergoeconomic analysis of hydrogen production using a standalone high-temperature electrolyzer - ScienceDirect</li> </ul> |



#### Algeria: Techno-economic study of hydrogen production using a hybrid nuclear-PV solar system CSI: Rafika BOUDRIES

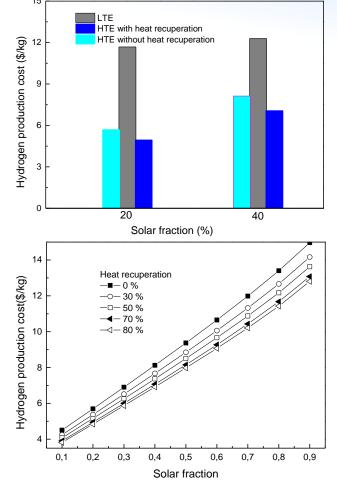


#### Centre de Développement des Energies Renouvelables (CDER)

- Cost analysis of nuclear-based hydrogen production by electrolysis
- Investigate competitiveness of nuclear-based hydrogen production with solar-based hydrogen production cost
- Techno-economic study of hydrogen production using a hybrid nuclear-solar system (HTR – solar PV) and SOEC for high temperature steam electrolysis

With establishment of relevant SOEC characteristic parameters

- Assessment of the evolution of
  - ✓ useful PV panel area with solar fraction and daily solar insolation
  - ✓ hydrogen production cost with solar fraction and daily solar insolation
  - hydrogen production cost with solar fraction and PV cell efficiency
- Study of the effect of heat recuperation on H cost
- Comparison of costs between HTSE obtained H and LTE obtained H



- Decrease in hydrogen production cost at HTE and this decrease increases with heat recuperation
- HTSE production more competitive than LTE.

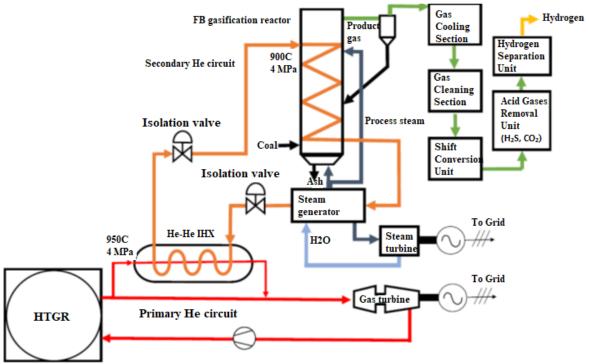
Hydrogen cost increases with increasing solar insolation at different heat recuperation fractions.

The cost of H production is highly affected by the solar fraction, and the solar irradiance on the PV panel. There are decreases in H production cost with increase either in PV cell efficiency, solar insolation or recuperation of the heat. The rate of decrease depends on the solar fraction.

# Argentina: Techno-economic feasibility study on the nuclear-assisted steam gasification of Argentine Rio Turbio coal for hydrogen production CSI: Ana BOHE

Comisión Nacional de Energía Atómica (CNEA)

- Evaluation of different HTGR designs to be potentially used as heat source for the nuclear-assisted steam gasification process
- Selection of the gasification technology to be implemented for processing the Rio Turbio coal in an indirectly heated gasification rector - High-Temperature Winkler (HTW) gasification process
- Heat balance analysis and sizing of an indirect-heating gasification reactor to be constructed as a Demonstration Plant, and critical evaluation of technical alternatives for upscaling the indirect-heating gasification reactor to a more commercial phase
- Evaluation of most critical safety issues for the coupling between the HTGR and the gasification plants
- Development of the plant layout for the safe coupling between a HTGR and a Demonstration Gasification Plant for hydrogen production
- preliminary calculations with the IAEA HEEP code to evaluate the economic feasibility of using a HTGR with 950°C core outlet temperature for electricity generation and hydrogen production through a nuclear-assisted Demonstration Gasification Plant in the Rio Turbio site



Layout of the Steam Gasification Demonstration Plant for processing the Rio Turbio coal for hydrogen production

Maximum thermal output of the gasification reactor is in the order of 10 MW



### China: Evaluation of MW Grade TMSR-Nuclear Hydrogen Production Using Solid Oxide Electrolysis Cell (SOEC) Technology



#### **CSI: Jian-Qiang WANG** Shanghai Institute of Applied Physics

- Study of material performance (SOEC)
  - ✓LSCF cathode material
  - ✓BZCY electrolyte material
  - ✓ Capacity of production in the range of kg
  - ✓ Development of anode supported cell
  - ✓Oxide coatings (e.g. Co-Mn-O spinel) to increase the service life
- Improvement of electrolysis performance of single cells and development of highperformance solid oxide stacks
  - ✓ Single stack scale: up to 7.2kW
  - ✓ Peak hydrogen production rate: ~2.3 Nm<sup>3</sup>/h
  - ✓ Electric consumption: ~3.2kWh/Nm<sup>3</sup>H<sub>2</sub>
  - ✓Tested stable operating time: ~ 3000 h
- Set up MW scale HTSE system
  - ✓ Completed the core design of 20kW, 200kW, and 2MW SOEC systems:
  - process flow, material and heat balance, long-period operating equipment data, process equipment, electrical load
  - ✓ Complete the core technical documents:
  - pipeline and instrument flow chart, electrical equipment specification, instrument general specification, pipeline stress specification
- System modelling for optimized heat integration technology •
- Coupling of the HTSE system with Thorium Molten Salt Reactor (TMSR) •
- Evaluation of economic and safety aspects of the TMSR nuclear hydrogen production plant • ✓ Safety analysis for molten salt long-distance heat transfer circuit used for coupling nuclear and HTSE system
  - ✓ Reducing the SOEC cost by improving the cell performance and service life, and scaling u





**Production Equipment of** Solid Oxide Cells and stacks

#### Construction of 20kW Hydrogen Production Pilot Program Based on SOEC Technology

|  |                                |                   | Parameters  | Value         |
|--|--------------------------------|-------------------|---|---------------|
|  |                                |                   | rated power   | 20 <u>KWe</u> |
|  |                                |                   | Operating<br>temperature  | 750 °C        |
| nal<br>control unit<br>iponents  |                                |                   | Hydrogen<br>production rate   | ~6 Nm3/h      |
| e the system   |                                |                   | Current density   | 0.25 A/cm2    |
| and debugging<br>erification of the<br>production and<br>ntegration system | AA                             |                   | Gas pressure  | ≤5 bar        |
|  |                                |                   | Daily Hydrogen  | ~10 kg/day    |
| actor ( including<br>Primary Loop)   | Secondary<br>Loop              | Third<br>Loop     | Fourth Loop : Electricity Generation<br>& Nuclear Heat Application System |               |
| Pump<br>D<br>H<br>H<br>X<br>X<br>e Core                                    |                                | Heat<br>Ecchanger | Sea Water<br>Desalitation<br>Turbine<br>Condensor                         |               |
|  | t and coolant<br>uclear reacto | Sait              | nal Energy Storage<br>r clean energy                                      |               |
|  |                                |                   | Non-electrical application  | n             |



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LCOH Results of MW-Scale MSRs Coupled with Hydrogen Production Based on SOEC

Technology

nology

| Power Plant Type                    | MSR      | MSR      |
|-------------------------------------|----------|----------|
| Thermal rating (MWth/unit)          | 300      | 600      |
| output temperature $tn^\prime$ (°C) | 650      | 650      |
| Heat for H2 plant (MWth/unit)       | 23       | 47       |
| SOEC Scale(MWe/unit)                | 127      | 262      |
| TH (MWe/unit)                       | 3        | 6        |
| H2 generation per unit (kg/yr)      | 3.21E+07 | 6.60E+07 |
| LCOH (\$/kg)                        | 3.85     | 3.83     |
|                                     |          |          |

for clean energy

Tool: HEEP

Nuclear Hydrogen with TMSR Nuclear Hydrogen

in nuclear reactor

### Greece: Identifying Adequate SMR Technology for Innovative Hydrogen Production, Compression and Storage CSI: Melpomeni VARVAGIANNI

National Center for Scientific Research "DEMOKRITOS"

- Investigate the appropriate solution for the energetic transition from lignite-fired power plants in the Western Macedonia Region (Northern Greece)
  - ✓ Selected SMR designs:
    - ≻CAP200 (China) PWR
    - ➢ International Reactor Innovative and Secure (IRIS) PWR
    - ➤ DMS (Japan) BWR
    - ➤IMR (Japan) PWR
    - ➤ VK300 (Russian Federation) BWR
    - ➤ Westinghouse SMR (USA) PWR
    - ➤ NUWARD (France)
- Selected the hydrogen storage method: metal hydrides
- performance of a cost analysis for a SMR and hydrogen electrolysis production with a MH compression system

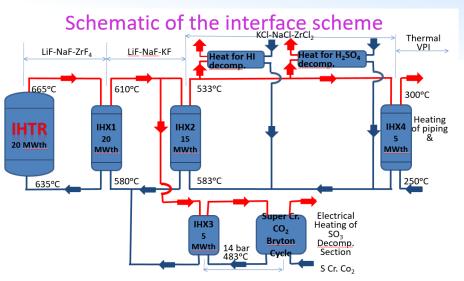
#### India: Technical and safety studies for integration of high temperature reactors with Iodine-Sulphur process based hydrogen production plant and upgradation of the IAEA software HEEP for economic assessment of hydrogen production CSI: Indravadan DULERA

#### Bhabha Atomic Research Centre (BARC)

- India has an active programme for development of the IS process.
- Closed loop operation demonstrated at 30 Nlph of H production
- Closed loop metallic system setup for 150 Nlph of H production
- New technologies developed:

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- ✓ multistage counter-current Bunsen reactor in tantalum
- ✓ membrane reactor for HI decomposition
- ✓ bayonet type SO<sub>3</sub> decomposer in silicon carbide
- √improved surface area catalyst for SO<sub>3</sub> decomposition
- Investigation of various options to couple 20 MWth Innovative High Temperature Reactor (IHTR) to the IS plant, while considering challenges related to heat transfer, material compatibility and code design requirements
  - ✓ IHTR is under design in India for demonstration of hydrogen production using IS process:
    - 20 MWth, molten salt cooled, pebble bed type reactor
    - Primary salt: LiF-NaF-ZrF4
    - Secondary salt: LiF-NaF-KF
    - Core inlet/outlet: 635 °C/665 °C
    - Moderator/reflector: Graphite
    - Structural material: Ni-Mo-Cr-Ti alloy
- Detailing of the selected design option for the intermediate heat exchangers and intermediate piping
- Identification of areas significant for safety studies
- Update of the HEEP tool



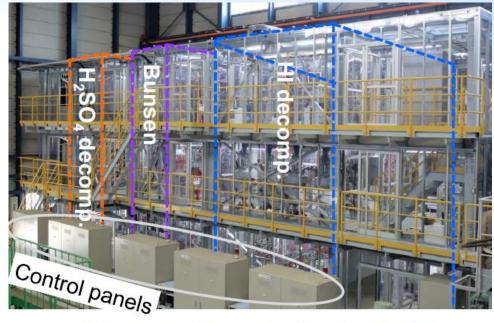
### Update of HEEP

- Included feature to generate report in Excel format
- Developed feature for studying sensitivity of specific parameter on hydrogen cost
- $\checkmark$  discount rate
- ✓ interest on borrowing
- ✓ equity
- ✓ construction period



#### Japan: R&D for IS thermochemical process for hydrogen production CSI: Xing YAN Japan Atomic Energy Agency (JAEA)

- Focus on R&D for thermochemical hydrogen production using the IS cycle to extend the period of stable hydrogen production at the facility and examine the integrity of the process reactors and components in high temperature and/or highly corrosive working conditions.
  - Long term continuous H production tests – at a rate up to 30 L/h
  - Acquiring corrosion data after the long-term H2 production tests
  - Investigation of structural materials for each process environment (H2SO4 decomposer, heat exchanger, Bunsen reactor, piping, HI decomposer) from corrosion tests



IS-process H<sub>2</sub> production test facility

#### National objective:

By 2030, to establish a coupling technology and perform hydrogen production tests at HTTR

### **Russian Federation: Assessing Potential of High Temperature Reactor Facilities** of Russian Design for Hydrogen Production

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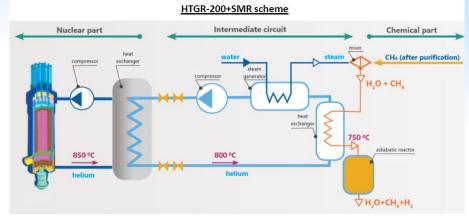


#### **CSI: Andrey BALANIN NRC Kurchatov Institute**

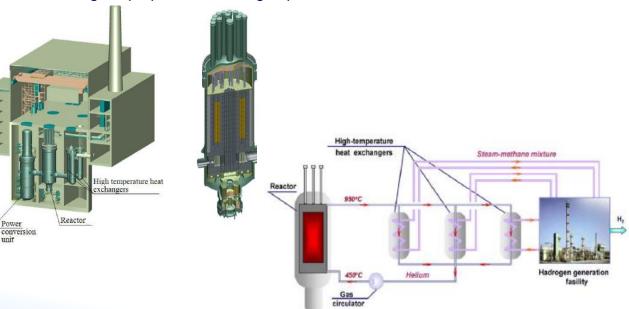
- Review of HTRs designed in Russia with potential for H ٠ production (HTGR, FGCR, MSR)
- MHR-T (600 MWt) and HTGR-200 (200 MWt) were selected for analysis, necessary data was collected
- Number of electrolysis facilities available on market ٠ selected for comparison, necessary data collected
- Models of technical-economic assessment of unit costs • of hydrogen production for selected facilities were developed
- Technical-economic assessments of hydrogen production ٠ were carried out for following cases:

✓ SMR and HTSE with MHR-T energy source of heat and electricity

- ✓ SMR with HTGR-200 energy source of heat
- ✓ Electrolysis and compression using electricity from outside source
- ✓ Simplified verifications of several cases with HEEP
- Approach of multi-criteria assessment of using nuclear reactors for H production was tested for several cases



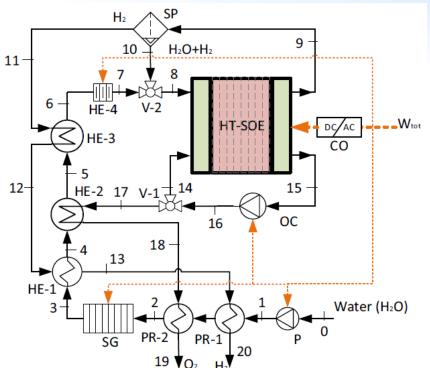
HTGR-200 + Steam Methane Reforming (SMR) is a latest design, developed by JSC Afrikantov OKBM based on MHR-100 design for power generation and technological purposes, including H production.





#### Saudi Arabia: Thermo-Economic Analysis and Optimization of a Large-Scale Nuclear Hydrogen Production Utilizing High Temperature Electyrolysis CSI: Abdullah ALZAHRANI Umm Al-Qura University

- Holistic plant model for hydrogen production comprising a nuclear reactor and an electrolysis component
- Adjusting of the critical cost and technical parameters considering WCR and HTGR technologies (APR 1400 and HTR-PM)
- Model for the SOE stacks
- Techno-economic analysis of integrating SOE plants with WCR and HTGR for large-scale hydrogen production



Schematic layout of the 1 MWe SOE hydrogen production plant

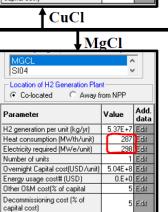
### **Turkey: Economics and Integration of Hybrid Thermochemical Cycles to Nuclear**

#### **Reactors for Hydrogen Production CSI: Hasan OZCAN Karabuk University**

- Development of hydrogen production plant ٠ configurations considering advanced reactor technologies (CANDU-SCWR and HTGR) with HyS, CuCl, MgCl and CaBr cvcles
- Performing thermodynamic and economic ٠ analysis to specify the most feasible options to be employed
- Effect of scaling of hybrid cycle configurations on H production costs
- Adapting the most feasible hybrid ٠ thermochemical cycles to IAEA-HEEP software package
- Comparative economic assessment of ٠ adapted hydrogen systems with storage and transportation

Cost comparison of the considered hybrid cycles with HTGR HyS cycle has the lowest hydrogen cost based on results with HEEP

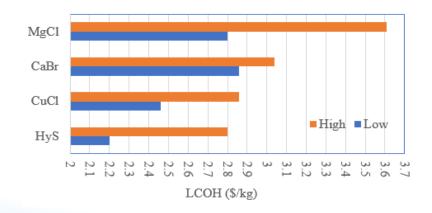
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|--|--------------|--------------|--|------------------------|--------------|
|  |              |              | Parameter  | Value                  | Add.<br>data |
|  |              |              | H2 generation per unit (kg/yr)   | 5.37E+7                | Edit         |
|  |              |              | Heat consumption (MW/th/unit)  | 308                    | Edit         |
| HTRG   |              |              | Electricity required (MW/e/unit)   | 133                    | Edit         |
|  |              |              | Number of units  |                        | Edit         |
| Parameter  | Value        | Add.         | Overnight Capital cost(USD/unit)   | 2.64E+8                | Edit         |
| Parameter  | value        | data         | Energy usage cost# (USD)   | 0.E+0                  | Edit         |
| Thermal rating (MWth/unit)   | 630.7        | Edit         | Other O&M cost(% of capital  | 5                      | Edit         |
| Heat for H2 plant (MWth/unit)  | 308          | Edit         | Decommissioning cost (% of   | 5                      | Edit         |
| Electricity rating (MWe/unit)  | 280          | Edit         | capital cost)  | 9                      | ЕСШ          |
| Number of units  | 2            | Edit         |  |                        |              |
| Initial fuel load (kg/unit)  | 18000        | Edit         | <b>†</b> CuCl  |                        |              |
| Annual fuel feed (kg/unit)   | 6000         | Edit         |  |                        | _            |
| Overnight Capital cost(USD/unit)   | 6.05E+8      | Edit         | <b>M</b>   | σCl                    |              |
|  |              |              |  | gui                    |              |
| Capital cost fraction for electricity<br>generating infrastructure (%)   | 25           | Edit         | MGCL   | ^                      |              |
| Capital cost fraction for electricity<br>generating infrastructure (%)   | 25<br>5535   |              | MGCL<br>SI04   | ~ ~                    |              |
| Capital cost fraction for electricity  | 25           | Edit         | SI04   | ~                      | ,            |
| Capital cost fraction for electricity<br>generating infrastructure (%)<br>Fuel cost (USD/kg)<br>D&M cost (% of capital cost)<br>Decommissioning cost (% of | 5535<br>5.75 | Edit         |  | v<br>nt                | ,            |
| Capital cost fraction for electricity<br>generating infrastructure (%)<br>Fuel cost (USD/kg)<br>D&M cost (% of capital cost)                               | 5535<br>5.75 | Edit<br>Edit | SI04   | v<br>nt                | Add.<br>data |
| Capital cost fraction for electricity<br>generating infrastructure (%)<br>Fuel cost (USD/kg)<br>D&M cost (% of capital cost)<br>Decommissioning cost (% of | 5535<br>5.75 | Edit<br>Edit | SID4<br>Location of H2 Generation Plat<br>Co-located C Away f<br>Parameter | nt<br>rom NPP<br>Value | Add.<br>data |
| Capital cost fraction for electricity<br>generating infrastructure (%)<br>Fuel cost (USD/kg)<br>D&M cost (% of capital cost)<br>Decommissioning cost (% of | 5535<br>5.75 | Edit<br>Edit | SI04<br>Location of H2 Generation Plan                                     | Value                  | Add.<br>data |



| Co-located C Away f   | rom NPP   |                      |
|---|---|----------------------|
| Parameter   | Value   | Ac<br>da             |
| H2 generation per unit (kg/yr)  | 5.37E+7   | Eε                   |
| Heat consumption (MWth/unit)  | 282   | 110                  |
| Electricity required (MWe/unit)   | 116   | l ie                 |
| Number of units   | 1   | Εe                   |
| Overnight Capital cost(USD/unit)  | 2.09E+8   | Εe                   |
| Energy usage cost# (USD)  | 0.E+0   | Εe                   |
| Other O&M cost(% of capital   | 5   | Εe                   |
| Decommissioning cost (% of capital cost)  | 5   | Ēε                   |
| HyS   | Br  | -                    |
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| HyS<br>HTSE04<br>HyS<br>Location of H2 Generation Plar<br>Co-located C Away fr<br>Parameter<br>H2 generation per unit (kg/yr)   | om NPP  | da<br>Ed             |
| HyS<br>HTSE04<br>HVS<br>Location of H2 Generation Plar<br>Co-located C Away fr<br>Parameter<br>H2 generation per unit (kg/yr)<br>Heat consumption (Mv/th/unit)  | om NPP<br>Value<br>5.37E+7<br>240                   | da<br>Ed             |
| HyS<br>HTSE04<br>HyS<br>Co-located Away fr<br>Parameter<br>H2 generation per unit (kg/yr)<br>Heat consumption (Mwth/unit)<br>Electricity required (Mw/e/unit)   | Value<br>5.37E+7<br>240<br>115.8                    | da<br>Ed             |
| HyS<br>HTSE04<br>HyS<br>Co-ation of H2 Generation Plar<br>Co-located Away fr<br>Parameter<br>H2 generation per unit (kg/yr)<br>Heat consumption (Mv/th/unit)<br>Electricity required (Mw/e/unit)<br>Number of units   | Value<br>5.37E+7<br>240<br>115.8                    | da<br>Ed<br>Ed       |
| HyS<br>HTSE04<br>HVS<br>Location of H2 Generation Plar<br>Co-located C Away fr<br>Parameter<br>H2 generation per unit (kg/yr)<br>Heat consumption (MW/th/unit)<br>Electricity required (MW/e/unit)<br>Number of units<br>Dvernight Capital cost(USD/unit)           | Value<br>5.37E+7<br>240<br>115.8<br>1.98E+8         | da<br>Ed<br>Ed<br>Ed |
| HyS<br>Location of H2 Generation Plar<br>Co-located Away fn<br>Parameter<br>H2 generation per unit (kg/yr)<br>Heat consumption (Mvth/vunit)<br>Electricity required (Mv/e/unit)<br>Number of units<br>Overnight Capital cost(USD/vunit)<br>Energy usage cost# (USD) | Value<br>5.37E+7<br>240<br>1158<br>1.98E+8<br>0.E+0 | da<br>Ed<br>Ed<br>Ed |
| HyS<br>HTSE04<br>HVS<br>Location of H2 Generation Plar<br>Co-located C Away fr<br>Parameter<br>H2 generation per unit (kg/yr)<br>Heat consumption (MW/th/unit)<br>Electricity required (MW/e/unit)<br>Number of units<br>Dvernight Capital cost(USD/unit)           | Value<br>5.37E+7<br>240<br>115.8<br>0.E+0<br>5      | da<br>Ed<br>Ed<br>Ed |

CE04

- Location of H2 Generation Plan



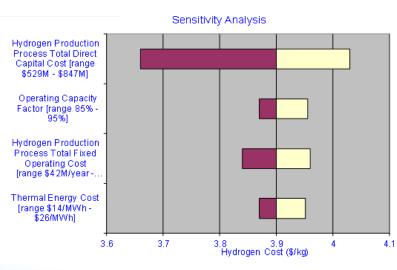
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#### United States: Safety and Scaling Analysis of Nuclear Hydrogen Production Schemes with Current and Near Future Nuclear Plants CSI: Shripad REVANKAR

**Purdue University** 

- Developed integrated dynamic model of Nuclear Reactor - Hydrogen Plants
   ✓HTGR and IS hydrogen production
  - ✓HTGR-HTE
  - ✓ LWR (PWR and BWR) LTE PEM Electrolyzer (Recent US Industry DOE Initiative)
  - ✓ Integrated Nuclear Renewable Energy System
- Scaling analysis for the integrated nuclear hydrogen production systems considering various nuclear reactor technologies
- Process flow diagrams for nuclear hydrogen system
- Techno-economic analysis of the integrated systems, comparison H2A results with HEEP results
  - Analysis Tools:
     First principle-based models for nuclear plants verified with codes: RELAP5, MELCOR
     Hydrogen Production Systems ASPEN PLUS
     Economic Analysis H2A, HEEP





#### H2A Analysis for HTE with HTGR 600MW

### From the CSIs:



"This precious opportunity in the CRP is unique for the researchers in SINAP to let more people know about our research and also gain insight in the related research conducted by the international community. It also provides an opportunity for development of our technologies and conduct additional research to investigate if the HTSE system is suitable while coupled with other energy sources such as wind, solar, Gen-III and some other Gen-IV reactors. Besides, the HEEP tool developed by IAEA simplifies the cost assessment of nuclear hydrogen production."

- Prof. Dr. Jian-Qiang Wang, Shanghai Institute of Applied Physics, China

"The theoretical feasibility study on nuclear-assisted gasification process applied to the Argentine Rio Turbio coal is very important for our country to provide the technical arguments needed during the decision making process regarding to the nuclear hydrogen production through the gasification of domestic coals. Aspects like the most convenient HTGR design, the maximum size of the gasification plant according to the present state of technologies, and the most critical safety issues to be considered for the coupling of the nuclear reactor and gasification plant, have been clarified through this study. Moreover, the experimental activities for pyrolysis and gasification tests conducted at bench-scale are also very important to evaluate the gasification behaviour of Argentine domestic coal in fluidized bed reactor conditions, as a function of the operational parameters (reaction temperature, partial pressure of reactive gases and coal particle size)."

- Dr. Ana Ester Bohé, Comisión Nacional de Energía Atómica (CNEA) de Argentina



# Questions?

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Thank you!